

IN THE SPECIFICATION:

Please replace the paragraph beginning at the bottom of page 7, line 24 to page 8, line 4, as follows:

Figure 2 shows a portion of a sub-assembly in accordance with the present invention comprising tubes (1) pierced with apertures (2) at their periphery at two levels: the number of aperture and the diameter is calculated as a function of the desired flexibility. A level of liquid is established. Its depth is generally in the range 50 to 200 mm. The depth of the downcomers is normally in the range 100 to 500 mm, preferably in the range 250 to 450 mm. The upper portions of these tubes are surmounted by caps (3) (jet disturber device) intended to break jets from either the inlet line or the upper bed of granular solid and to enable the gas and liquid to separate. The tubes extend (4) beyond the base of tray (P) by a depth that is normally in the range 20 to 100 mm. Liquid penetrates into the tube via the apertures and gas enters via the upper portion (22). The interior of the downcomer is filled over a depth that is more than the distance between the aperture (2) closest to tray (P) and the aperture (2) furthest away from this tray (P) with a Sulzer type packing (5) sold under reference number SMV. This packing is characterized in that it is constituted by at least one element wherein the cross section of flow is essentially transverse to the vessel axis, this element extending over the whole transverse cross section of the vessel in the circulation zone and being constituted by cells through which the process liquid, the process gas and the quench fluid pass, these cells orientating the fluid circulation in a substantially radial direction. The two-phase mixture formed in tube (1) leaves via the lower end (23) of this tube.

Please replace the paragraph beginning on page 9, line 7, with the following amended paragraph:

Figure 5b shows a vessel containing a plurality of catalyst beds containing a sub-assembly of the present invention which in addition to improving distribution (increasing the spray effect) can minimize the space taken up by the internal means in the reactor by using a one-stage tray (55) (no double-pass tray or mixing chamber). The elements designated by the same reference

numbers as those shown in Figures 2 and 5a are identical to those described with respect to these figures. The geometry of jet disturber device (3) is different from that shown in Figure 2. This jet disturber device is a deflector fixed on the tube (1) that forms an inlet that is skewed with respect to the top and bottom of tube (1).